

Review quiz

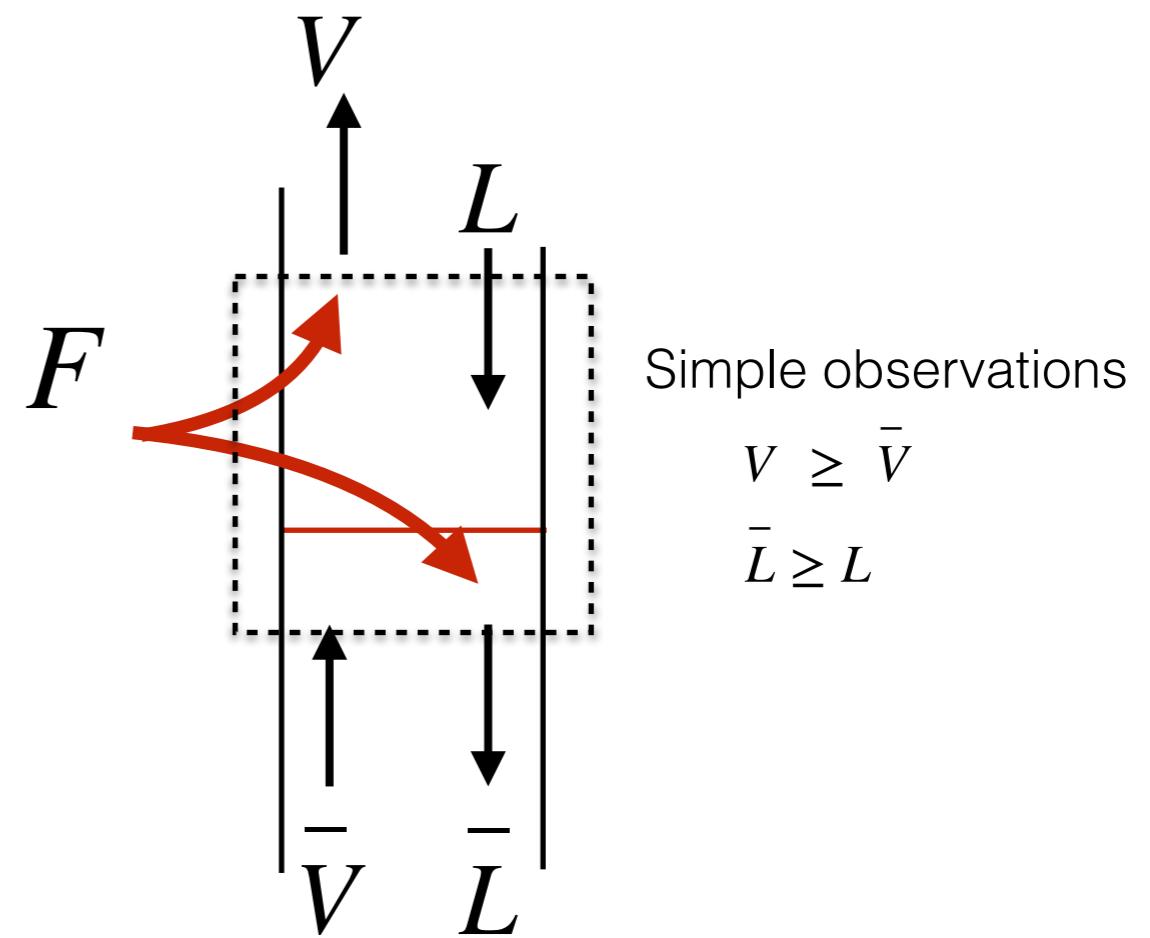
You are adding a saturated liquid feed $F = 100$. Calculate $\bar{L} - L$.

A. 50

B. 0

C. 100

D. -100



Review quiz

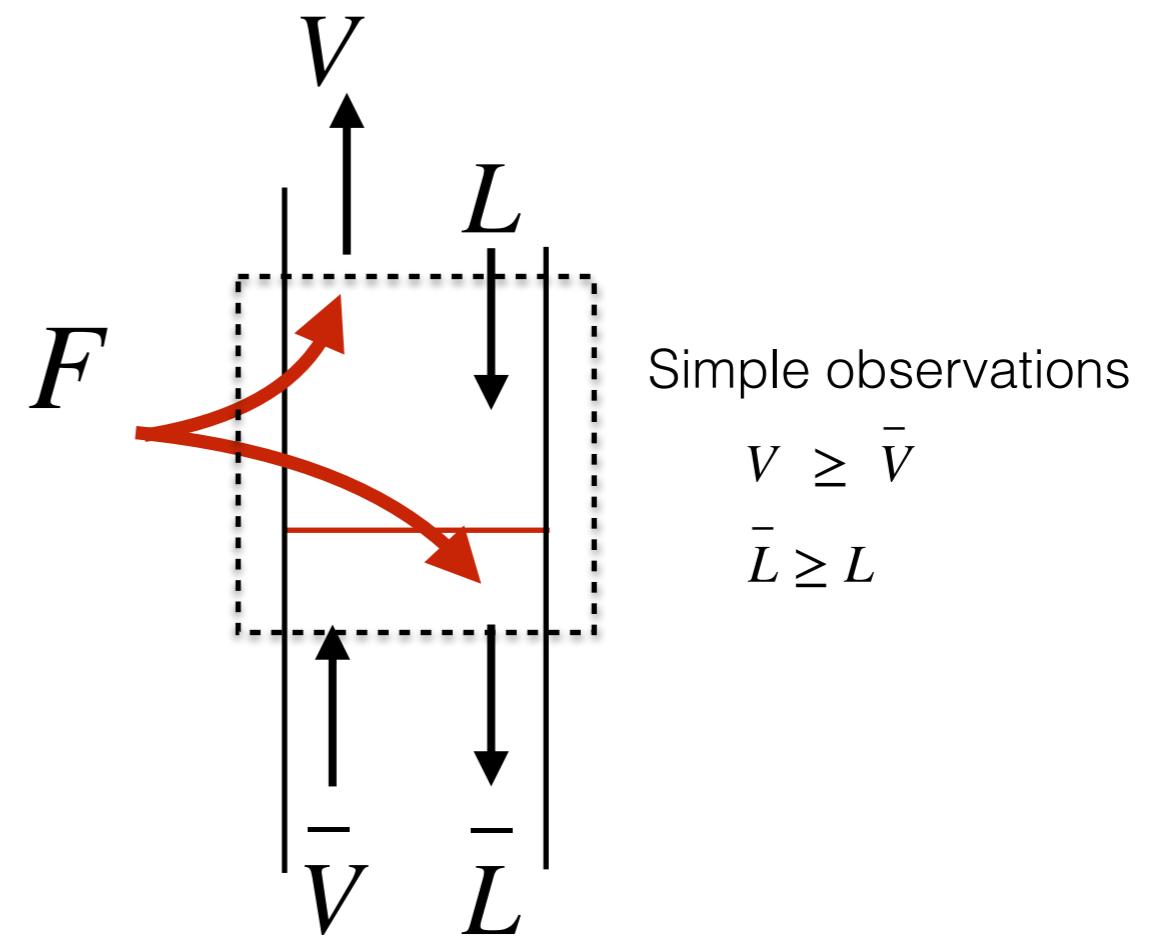
You are adding a saturated vapor feed $F = 100$. Calculate $\bar{V} - V$.

A. 50

B. 0

C. 100

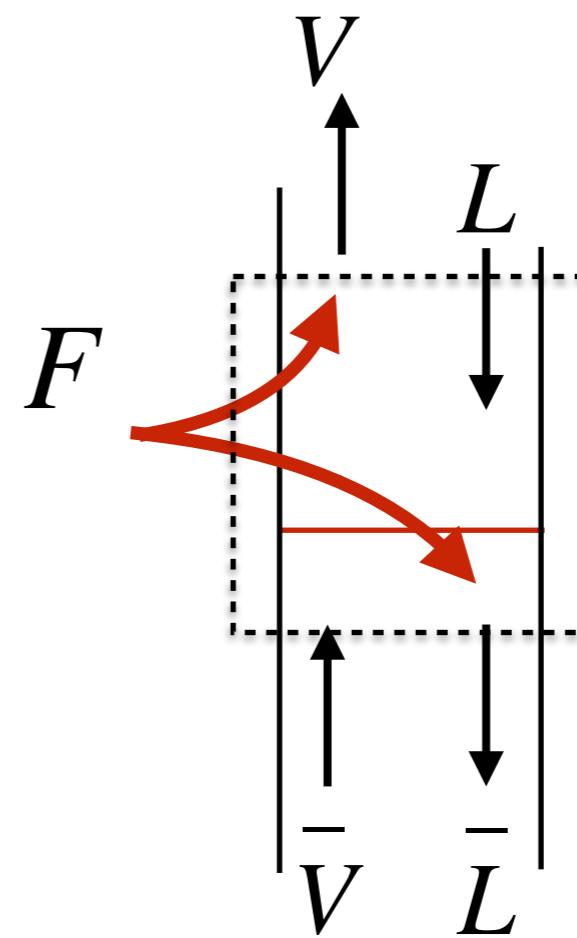
D. -100



Review quiz

You are adding a subcooled liquid feed. Which of the following is NOT true.

- A. $q > 1$
- B. $\bar{L} - L > 0$
- C. $\bar{V} - V > 0$
- D. $\bar{L} - L = F$



Simple observations
 $V \geq \bar{V}$
 $\bar{L} \geq L$

Review quiz

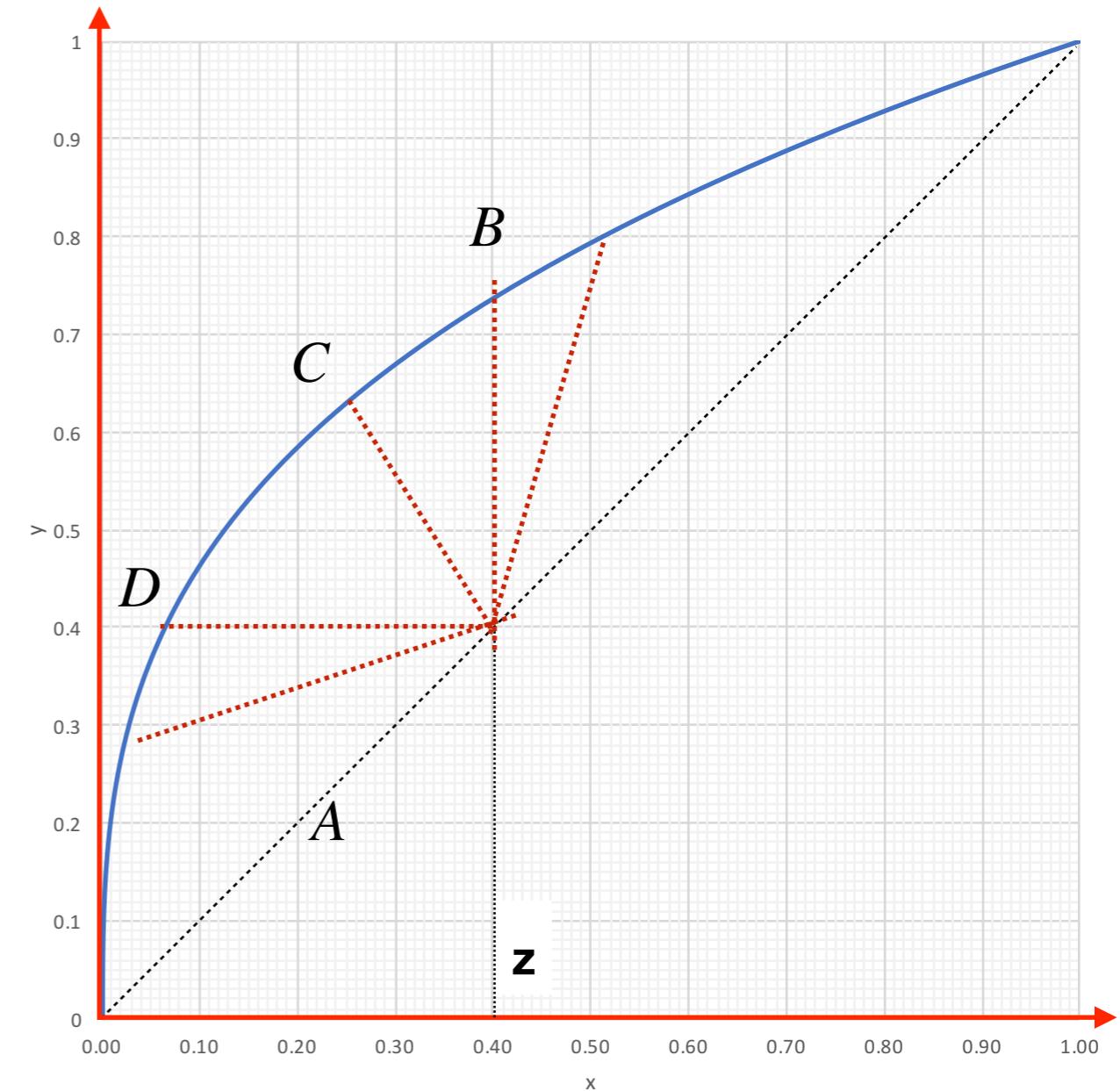
Which one of the following is saturated liquid feed line

A .

B .

C .

D .



Review quiz

What happens when you decrease the reflux ratio R to minimum, R_{min}

A . Number of stages $\rightarrow \infty$

B . $B \rightarrow \infty$

C . $F \rightarrow 0$

D . $D \rightarrow \infty$

Review quiz

What happens when you increase the reflux ratio R to maximum, ∞

- A* . Number of stages are maximized
- B* . L is minimized
- C* . The slope of both operating lines becomes 1
- D* . None of the above

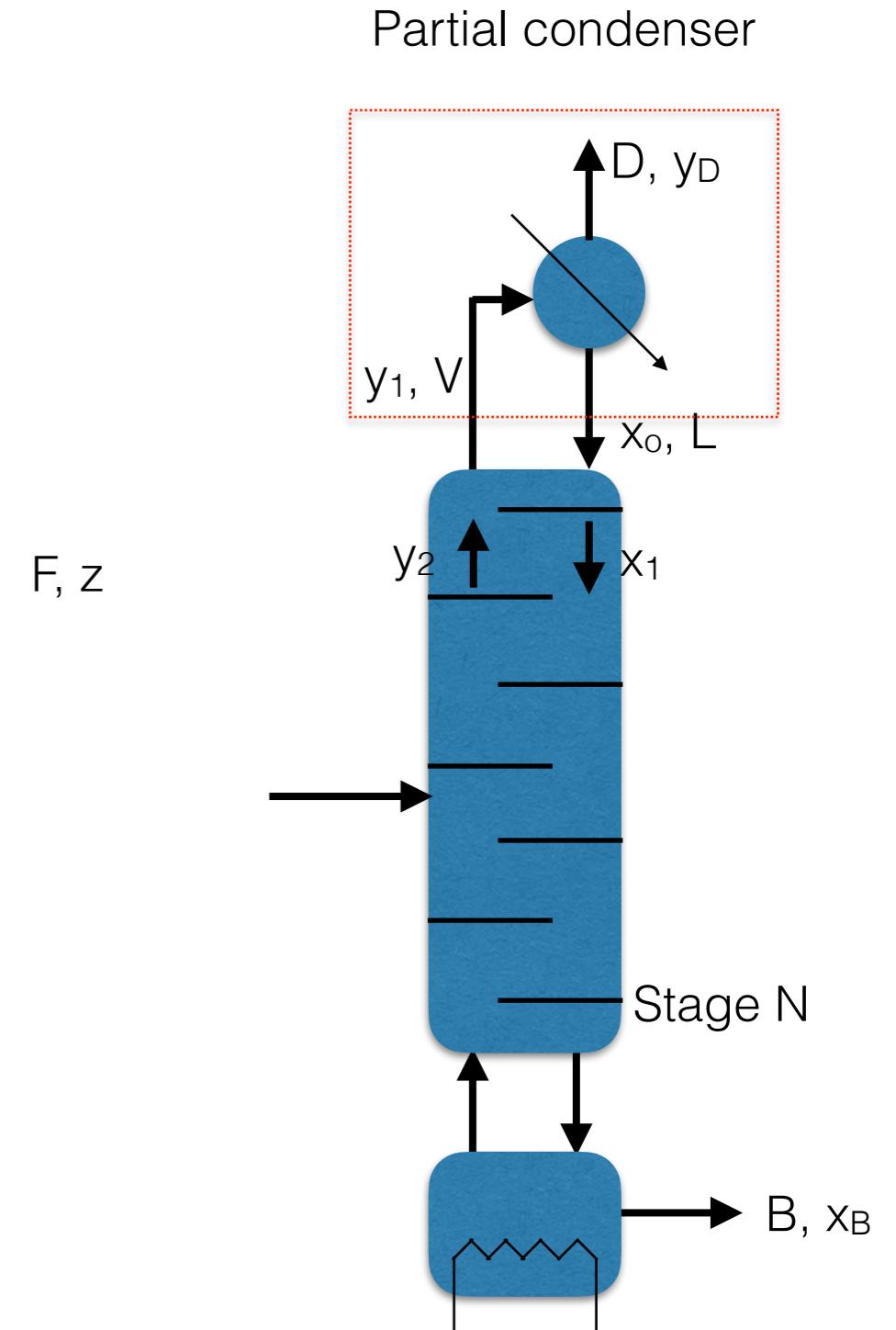
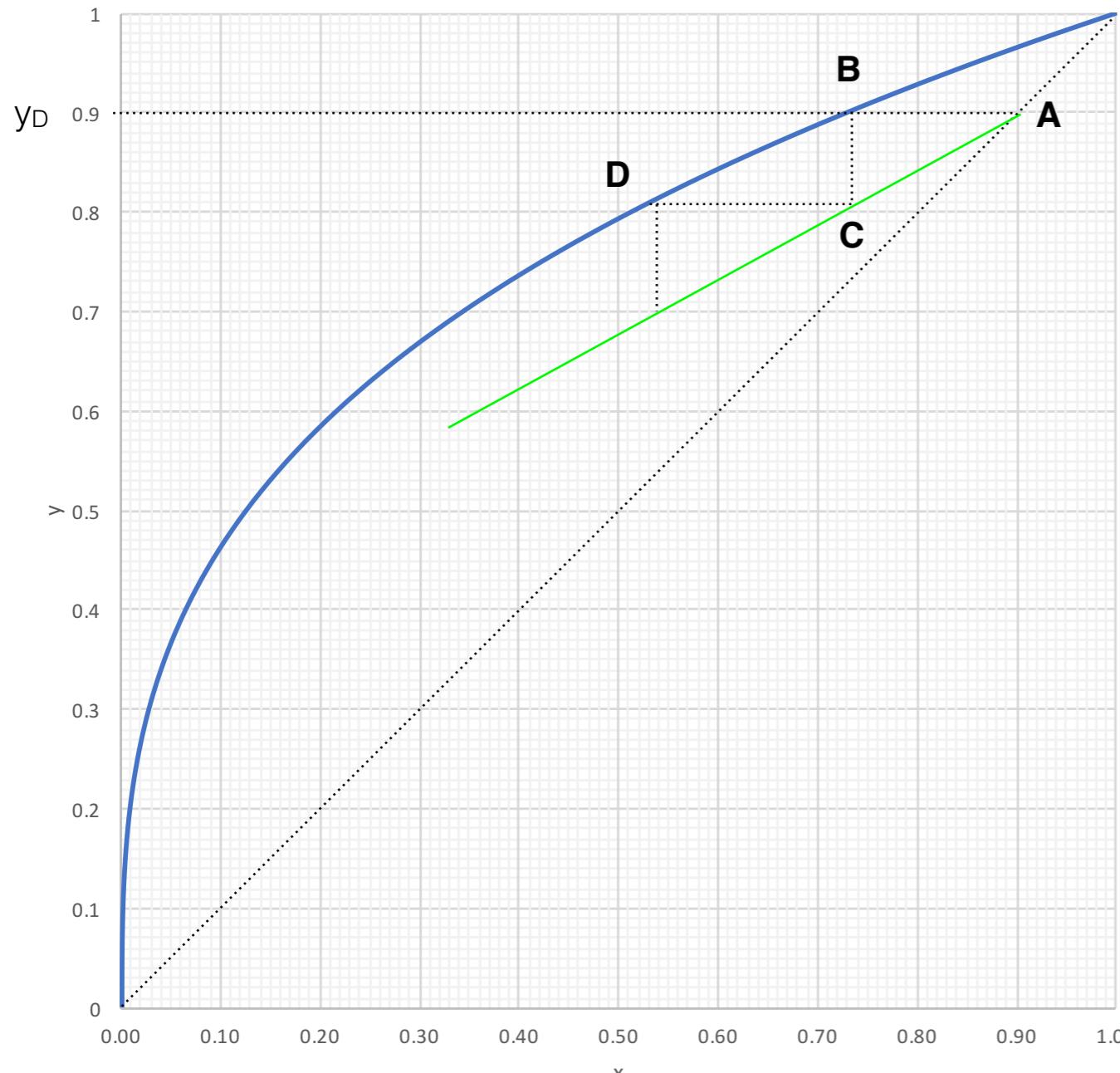
Review quiz

You decided to replace a total condenser by a partial condenser. What will happen to the total number of equilibrium stages

- A . They will stay the same**
- B . They will increase by 1**
- C . Total number of equilibrium stages will have to be determined by new operating lines**
- D . None of the above**

Review quiz

Which points on the plot represent (x_1, y_1)

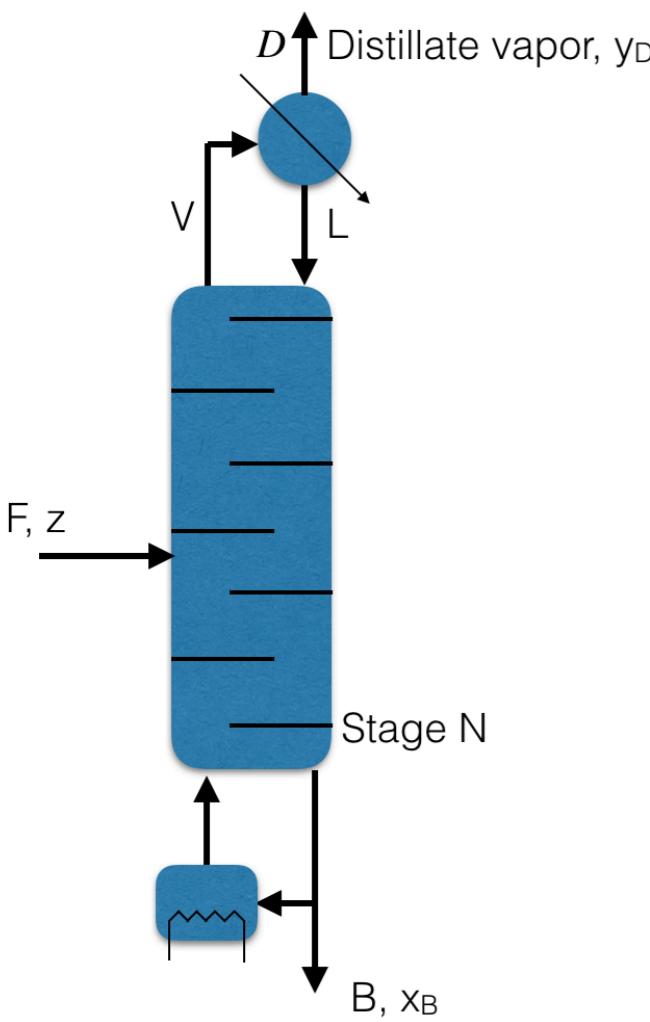


In-class Exercise problem

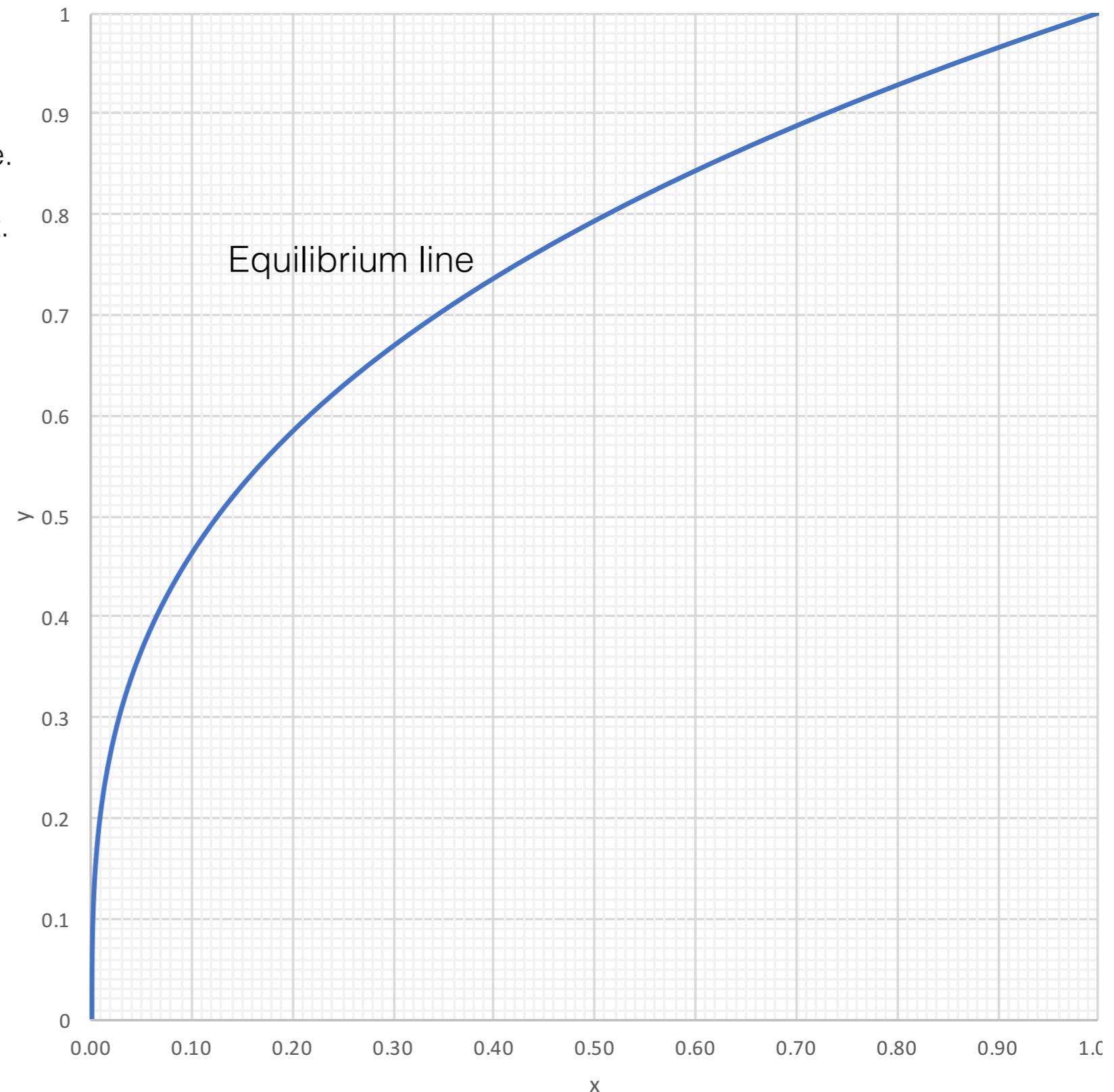
Consider the separation of binary mixture in saturated vapor state with a distillation column using partial condenser and a total reboiler. Feed flow rate ($z_1 = 0.5$) is 100 mol/hr. Your target is to recover 90% of the more volatile component (component 1) of the feed in the distillate. If reflux ratio is set to 1.5 times minimum reflux ratio, and $D = 50$ mole/hr, calculate:

- 1) Minimum reflux ratio.
- 2) Equation of rectifying section's operating line.
- 3) Total number of stages.
- 4) Highlight (x_0, y_D) , (x_1, y_1) , (x_2, y_3) in the plot.

Partial condenser



Total reboiler



$$F = 100 \text{ mole/hr}$$

$$z = 0.5$$

$$y_D = 45/50 = 0.9$$

$$B = F - D = 100 - 50 = 50$$

$$Bx_B + Dy_D = Fz$$

$$\Rightarrow B = F \frac{y_D - z}{y_D - x_B}$$

$$x_B = 0.1$$

Feed is saturated vapor; $q = 0$

$$\frac{R_{min}}{R_{min} + 1} = \frac{0.90 - 0.5}{0.90 - 0.125} = 0.516$$

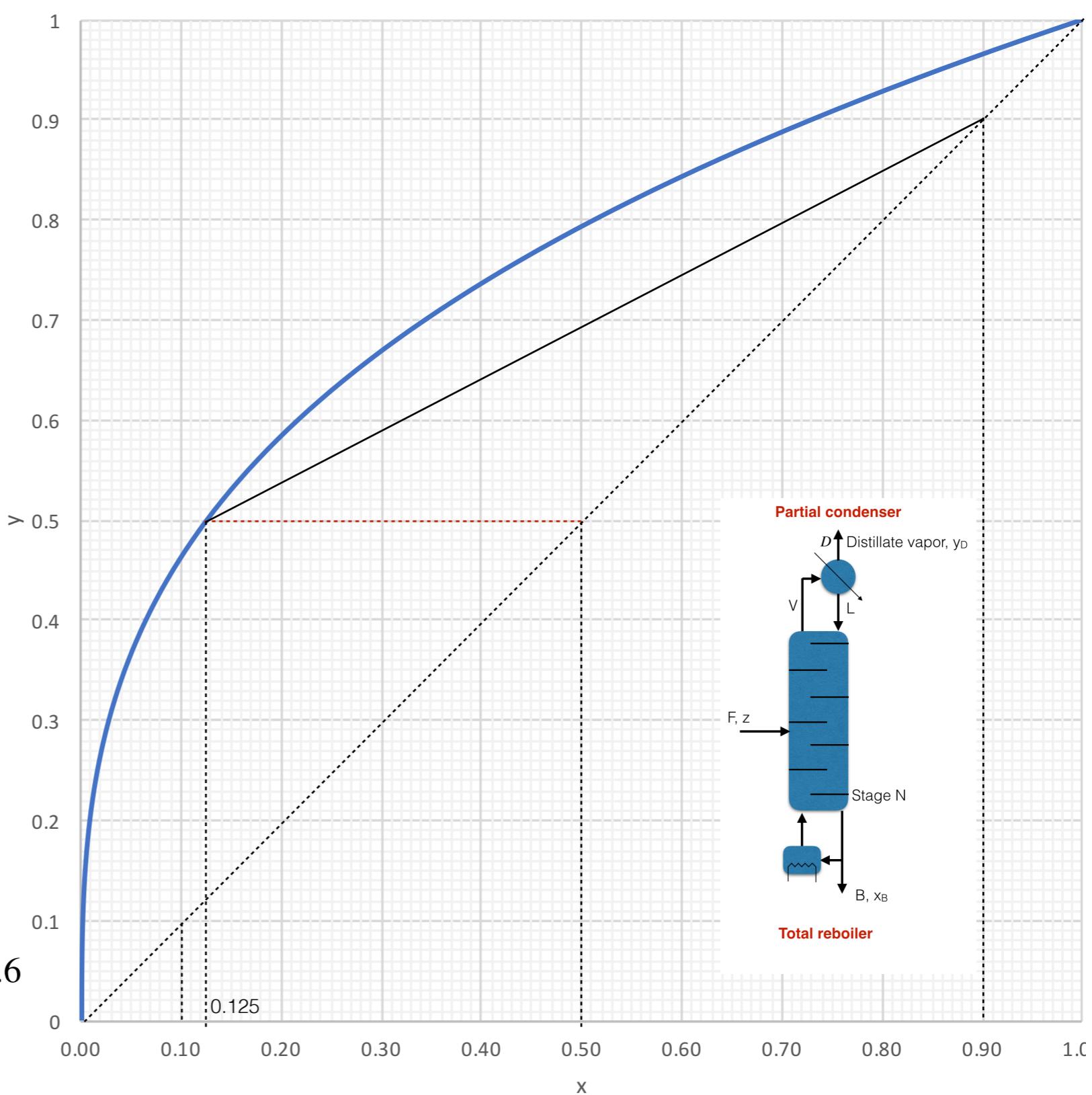
$$R_{min} = 1.066$$

$$R = 3R_{min} = 3.198$$

$$\Rightarrow \frac{R}{R + 1} = 0.6$$

Amount of component 1 in feed = $100 * 0.5 = 50 \text{ mole/hr}$

Amount of component 1 in distillate = $50 * 0.9 = 45 \text{ mole/hr}$



$$\Rightarrow \frac{R}{R+1} = 0.6$$

Operating line for rectifying section

$$y = 0.6x + c$$

$$c = 0.9 - 0.6 \cdot 0.9 = 0.36$$

$$y = 0.6x + 0.36$$

**Total number of stages = 5
(including partial condenser)**

